

EXAMPLE: DESIGN OF CSTR WITH BIOMASS RECYCLE

Oxygen supply is an important constraint for process design.

- Oxygen transfer through conventional aeration devices is limited, with 1,000 g-O₂/m³-d to be assumed to be a maximum rate of oxygen supply
- Aeration via compressed air supplied by mechanical blowers (bubble) or turbines is costly – especially in terms of energy consumption

Purpose of this example: develop a CSTR-biomass recycle process to minimize plant size while maintaining oxygen requirement < 1,000 g-O₂/m³-d.

Given

$$S_{SO} = 250 \text{ g/m}^3 \text{ COD}$$

$$S_S \leq 10 \text{ g/m}^3 \text{ COD} \quad (\text{discharge permit})$$

$$S_{NHO} = 40 \text{ g/m}^3 \text{ NH}_4\text{-N}$$

$$S_{NH} \leq 0.5 \text{ g/m}^3 \text{ NH}_4\text{-N}$$

Kinetic and stoichiometric data,

$$\hat{\mu}_H = 4 \text{ d}^{-1}$$

$$\hat{\mu}_A = 1 \text{ d}^{-1}$$

$$K_S = 25 \text{ g/m}^3 \text{ COD}$$

$$K_{NH} = 3 \text{ g/m}^3 \text{ NH}_4\text{-N}$$

$$b = 0.05 \text{ d}^{-1} \text{ for both heterotrophs and nitrifiers}$$

$$Y_H = 0.64 \text{ g-heterotrophic cell COD/g-substrate COD}$$

$$Y_A = 0.12 \text{ g- autotrophic cell COD/g- NH}_4\text{-N}$$

$$f_D = 0.2 \text{ g-debris COD/g-biomass COD decayed}$$

$$i_{NXB} = i_{NXD} = 0.09 \text{ g- NH}_4\text{-N/g-cell COD}$$

$$\mu_H = \hat{\mu}_H \frac{S_S}{(K_S + S_S)}$$

$$\mu_A = \hat{\mu}_A \frac{S_{NH}}{(K_{NH} + S_{NH})}$$

assume $X_{BA} \ll X_{BH}$ and nitrogen synthesis requirement to autotrophs can be neglected

1. Relation between Θ and S_S and S_{NH}

For $\Theta > 0.5$ d, discharge permit for COD is satisfied.

For $\Theta > 11$ d, discharge permit for ammonia-nitrogen is satisfied.

2. Relation between Θ and X_{BH}

Recall that the product $X_{BH}\tau$ = function of (Θ) and decreases as Θ increases. Also products $X_D\tau$ and $X_T\tau$ both increase as Θ increases.

3. OXYGEN CONSTRAINT for design of CSTR

$$r_{O,max} = RO/V = 1,000 \text{ g-O}_2/\text{m}^3\text{-d}$$

Note that minimum volume of CSTR is achieved at minimum $\tau = \tau_{min}$.

for COD oxidation only,

$$\tau_{min} = \frac{1}{r_{O,max}} \left[(S_{SO} - S_S)(1 - Y_{HOBS}) \right]$$

and $X_{max} = (X\tau) / \tau_{min}$ where $X\tau = X\tau(\Theta)$

4. Other constraints:

$$3 \text{ days} < \Theta$$

$$X_T > 1,500 \text{ g/m}^3 \text{ COD}$$

5. Adding nitrification

$$\tau_{min} = \left(\frac{1}{r_{O,max}} \right) \left[(S_{SO} - S_S)(1 - Y_{HOBS}) + 4.57 \left[(S_{NHO} - S_{NH}) - i_{NXB} Y_{Hobs} (S_{SO} - S_S) \right] \right]$$

6. Note that wasting rate, observed yield and nitrogen synthesis requirements all decrease as Θ increases