

# Homework 9 solutions

1. ideal pump is isentropic (adiabatic & reversible)

since for liquid  $s_2 - s_1 = C_p \ln(\frac{T_2}{T_1})$  it is also isothermal

2. boiling water at constant pressure is isothermal and internally, BUT NOT externally, reversible

3. turbine is isentropic only if it is adiabatic and reversible

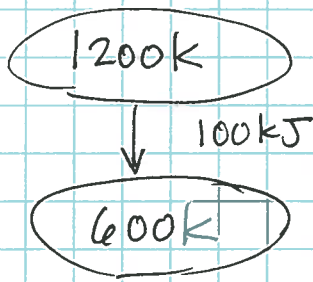
4. for  $s_2 - s_1 = 0$  and  $S_{gen} > 0$

$$S_{gen} = -\frac{\dot{Q}}{T} \text{ and } -\frac{\dot{Q}}{T} > 0$$

so system must lose heat

5.  $s_2 - s_1 = S_{gen}$  AND  $s_2 > s_1$

6.



for reservoir

$$\Delta S = \frac{\dot{Q}}{T} \text{ OR } \frac{Q}{T} = \Delta S$$

$$\Delta S_{HTR} = \frac{-100 \text{ kJ}}{1200 \text{ K}} = -0.0833 \frac{\text{kJ}}{\text{K}}$$

$$\Delta S_{LTR} = \frac{+100}{600 \text{ K}} = 0.167 \frac{\text{kJ}}{\text{K}}$$

$$\Delta S_{sys} = -0.0833 + 0.167 = \boxed{0.0833 \frac{\text{kJ}}{\text{K}}}$$

# 7. CARNOT Heat pump

(2)

$$\dot{Q}_H = 100 \text{ kW} \quad T_H = 21^\circ\text{C} = 294 \text{ K}$$

$$T_L = 10^\circ\text{C} = 283 \text{ K}$$

$$a) \text{ COP} = \frac{1}{1 - \frac{T_L}{T_H}} = \frac{1}{1 - \frac{283}{294}} = 26.7$$

$$26.7 = \frac{100 \text{ kW}}{\dot{W}} \quad \dot{W} = 3.74 \text{ kW}$$

$$\dot{Q}_L = -3.74 \text{ kW} - (-100 \text{ kW})$$

$$= 96.3 \text{ kW}$$

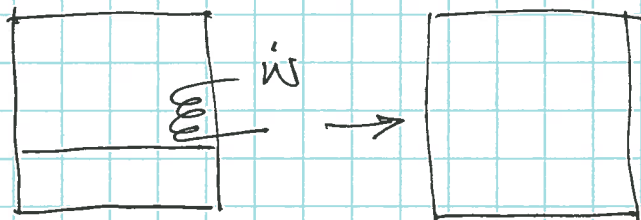
$$\Delta S_{HTR} = -\frac{100 \text{ kW}}{294 \text{ K}} = -0.34 \frac{\text{ kW}}{\text{K}}$$

$$\Delta S_{LTR} = \frac{96.3}{283} = +0.34 \frac{\text{ kW}}{\text{K}}$$

$$\dot{S}_{gen} = -\sum_k \left( \frac{\dot{Q}_k}{T_k} \right) = -0.34 - (-0.34)$$

Satisfies CAUSUS  $-\sum_k \left( \frac{\dot{Q}_k}{T_k} \right) \leq 0$   
 (= 0 for reversible cycle)

8.



$$m = 2 \text{ kg}$$

$$X_1 = 0.25$$

$$P_1 = 100 \text{ kPa}$$

$$X = 1$$

~~$$P_2 = 100 \text{ kPa}$$~~

$$S_2 = S_g @ T_2$$

$$P_2 = 439 \text{ kPa} \leftarrow$$

$$v_2 = v_1$$

$$v_1 = 0.25(v_{fg}) + v_f @ 100 \text{ kPa}$$

$$= 0.25(1.6941) + 0.001043$$

$$v_2 = 0.4246 \text{ m}^3/\text{kg}$$

$$= v_g \Rightarrow \text{interpolate for } P_2 \text{ to set } S_2$$

$$400 < P_2 < 450$$

$$P_2 - 400 = \frac{0.4246 - 0.46242}{0.41392 - 0.46242} \times 50$$

8.

$$\frac{439 - 400}{450 - 400} = \frac{s_2 - 6.8955}{6.8561 - 6.8955}$$

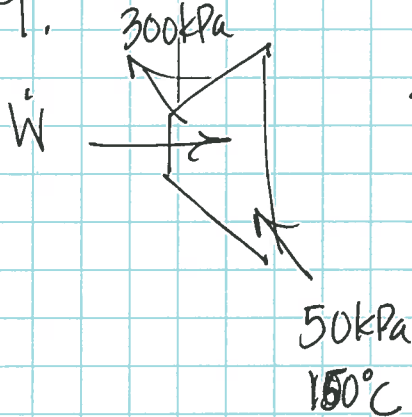
$$s_2 = 6.8648 \frac{\text{kJ}}{\text{kg K}}$$

$$s_1 = 0.25(s_{fg}) + s_f @ 100 \text{ kPa} \\ = 0.25(6.0562) + 1.3028 = 2.8169 \frac{\text{kJ}}{\text{kg K}}$$

$$m \Delta s = (s_2 - s_1) m = 2 \text{ kg} (6.8648 - 2.8169) \frac{\text{kJ}}{\text{kg K}}$$

$$\Delta S = 8.1 \frac{\text{kJ}}{\text{K}}$$

9.



steam in adiabatic + reversible  
compressor

$$s_2 = s_1$$

$$-\dot{W} = \dot{m}(h_2 - h_1)$$

$$-w = h_2 - h_1$$

a)

$$s_1 = 7.9413 \frac{\text{kJ}}{\text{kg K}} = s_2 @ 300 \text{ kPa } s_2 > s_g \text{ (still superheated)}$$

$$\frac{T_2 - 300}{400 - 300} = \frac{7.9413 - 7.7037}{8.0347 - 7.7037}$$

$$T_2 = 371.8^\circ \text{C}$$

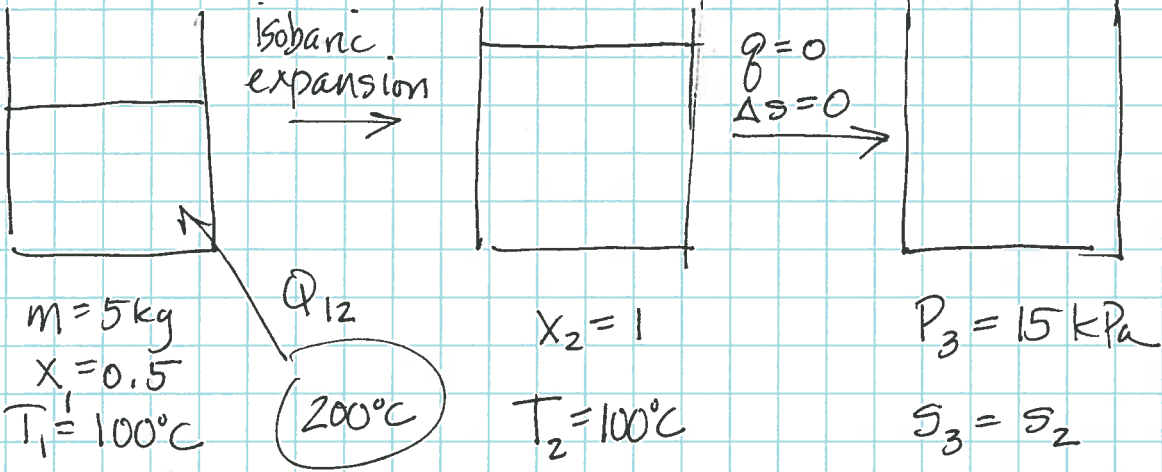
b)

$$\frac{h_2 - 3069.6}{3275.5 - 3069.6} = \frac{371.8 - 300}{100}, h_2 = 3217.4 \frac{\text{kJ}}{\text{kg}}$$

$$-W = 3217.4 - 2780.2 = 437.2 \frac{\text{kJ}}{\text{kg}} \text{ input}$$

10.

3



$m = 5 \text{ kg}$   
 $X = 0.5$   
 $T_1 = 100^\circ\text{C}$

$Q_{12}$   
 $200^\circ\text{C}$

$X_2 = 1$   
 $T_2 = 100^\circ\text{C}$

$P_3 = 15 \text{ kPa}$   
 $S_3 = S_2$

$S_1 = 0.5(s_{fg}) + s_f$   
 $@ 100^\circ\text{C} = 0.5(6.047) + 1.3072 = 4.33 \frac{\text{kJ}}{\text{kg}}$

$S_2 = S_g @ 100^\circ\text{C}$

Diagram:  $S_2 = 7.3542 = S_g = S_3 @ 15 \text{ kPa}$   
 $@ 100^\circ\text{C}$

	T	S
1	100	4.33
2	100	7.35
3	54	7.35

$s_f < s_3 < s_g @ 15 \text{ kPa} \Rightarrow \text{sat. mixture}$

$T_3 = T_s = 54^\circ\text{C}$

$X_3 = (7.3542 - 0.7549) / 7.2522 = 0.91$

$Q_{12} = m(h_2 - h_1)$       $h_1 = 0.5(2256.4) + 419.17 = 1547.9 \text{ kJ/kg}$

b.  $Q_{12} = 5 \text{ kg} (2675.6 - 1547.9) = 5,638.5 \text{ kJ}$

$h_2 = h_g @ 100^\circ\text{C} = 2675.6 \text{ kJ/kg}$

$h_3 = 0.91(2372.3) + 225.94 = 2384.7 \text{ kJ/kg}$

c.  $-W = m(h_3 - h_2) = 5 \text{ kg} (2384.7 - 2675.6)$

$W = 1,454.7 \text{ kJ}$

11. a)  $\sum_k \left(\frac{\dot{Q}}{T}\right)_k \leq 0$  (Clausius)

$\dot{Q}_H = -25 \text{ kW}$   
 $\dot{W} = -5 \text{ kW}$

$-5 \text{ kW} = -25 \text{ kW} + \dot{Q}_L$

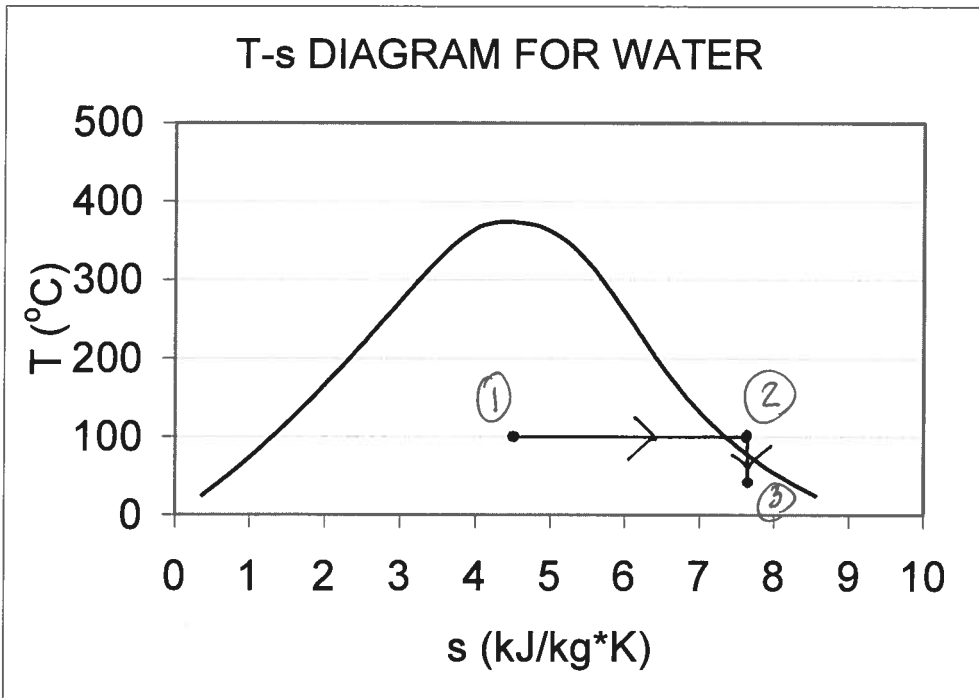
$\dot{Q}_L = 20 \text{ kW}$

$-\frac{25 \text{ kW}}{300 \text{ K}} + \frac{20 \text{ kW}}{260 \text{ K}} = -0.0064 \leq 0 \checkmark$

b)  $\text{COP}_{\text{COP}} = \frac{1}{1 - T_L/T_H} = 7.5$ ,  $\text{COP} = \frac{25}{5} = 5 < \text{COP}_{\text{COP}} \checkmark$

c)  $\dot{S}_{\text{gen}} = -\sum_k \left(\frac{\dot{Q}}{T}\right)_k = -(-0.0064) = 0.0064 \frac{\text{kJ}}{\text{K}}$

a. Draw the process on the T-s diagram below



- b. Determine the heat transfer in process 1→2 in kJ.
- c. Determine the work done in process 2→3 in kJ.
- d. What is the change in entropy in the surroundings for the two-step process in kJ/K?

11. (7 points, 3 for a and 2 each for b and c) A heat pump design is proposed that provides 25 kw heat while consuming 5 kw electrical power. The high- and low-temperature reservoirs are 300K and 260K, respectively.

- a. Show that the cycle satisfies Clausius' principle.
- b. Show that the cycle satisfies Carnot's principle.
- c. What is the entropy produced in the surroundings (kw/K)?