Work and 1st Law notes

Work, W = all energy transferred across boundary, <u>EXCEPT</u> heat

BOUNDARY WORK

Boundary Work = $W_b = \int P dV_{(kJ)}$ <u>Special cases:</u> Isobaric: $w = P(v_2 - v_1)$ (kJ/kg) Isochoric: w = 0Isothermal, ideal gas (Pv = C): $w = RT \ln\left(\frac{v_2}{v_1}\right) = RT \ln\left(\frac{P_1}{P_2}\right) = P_1V_1 \ln\left(\frac{v_2}{v_1}\right)$ (kJ/kg) Polytropic, gas ($Pv^n = C$): $w = \frac{P_2v_2 - P_1v_1}{(1-n)}$ (kJ/kg)

FIRST LAW

ENERGY PROPERTIES Internal Energy, U and enthalpy, H

Ideal gases

$u_2 - u_1 = C_V^*(T_2 - T_1)$	(kJ/kg)
$h_2 - h_1 = C_P^*(T_2 - T_1)$	(kJ/kg)

<u>Ideal liquids</u>: $C_V = C_P$ and $h_2 - h_1 = u_2 - u_1$

Water/steam and refrigerant: Use tables A-4 – A-6 and A-11 – A-13.

Closed System

General:

 $\mathbf{Q} - \mathbf{W} = \Delta \mathbf{U}$

Sign convention: Work done by (out of) system (+). Heat into system (+).

Special Cases

$Q - W_b = \Delta U \text{ OR } Q = \Delta H$
$-\mathbf{W} = \Delta \mathbf{U}$
$\mathbf{Q} = \Delta \mathbf{U}$
$0 = \Delta U$
$\mathbf{Q}_{\text{net}} = \mathbf{W}_{\text{net}}$

Open systems at STEADY STATE

$$\dot{Q} - \dot{W} = \sum_{e} \dot{m}_{e} (h_{e} + \frac{V_{e}^{2}}{2} + gz_{e}) - \sum_{i} \dot{m}_{i} (h_{i} + \frac{V_{i}^{2}}{2} + gz_{i}) \quad (kw)$$

<u>Special Cases</u> one inlet (1) and one outlet (2)

$$\dot{Q} - \dot{W} = \dot{m}(h_2 - h_1 + \frac{(V_2^2 - V_1^2)}{2000} + g(z_2 - z_1))$$
 (kw)

where units of h are kJ/kg, V are m/s and z is km

neglecting potential energy changes (nozzles, diffusers)

$$\dot{Q} - \dot{W} = \dot{m}(h_2 - h_1 + \frac{(V_2^2 - V_1^2)}{2000})$$
 (kw)

Stationary - ke and pe changes neglected: (often turbines, compressors).

$$\dot{Q} - \dot{W} = \dot{m}(h_2 - h_1)$$
 (kw)

Adiabatic and passive, no heat or work (often heat exchangers, mixers)

$$0 = \sum_{e} \dot{m}_{e}(h_{e}) - \sum_{i} \dot{m}_{i}(h_{i}) \qquad (kw)$$

adiabatic throttling value: $h_2 = h_1$

Cycle:

$$\dot{Q}_{net} = \dot{W}_{net}$$
 (kw)

mass flow rate, \dot{m} :

Conservation of mass at steady-state: $\sum_{i} \dot{m}_{i} = \sum_{e} \dot{m}_{e}$

$$\dot{m} = \rho VA = \rho \dot{V} = \frac{\dot{V}}{v}$$
 where $V =$ velocity, $v =$ spec. vol., $\dot{V} =$ vol. flow rate

Individual control volume devices – see handout on web page.

Problem Solution Rubric:

- 1. Write the 1st law for the appropriate system.
- 2. Modify 1st law for special cases
- 3. Calculate energy properties (internal energy, enthalpy) using specific heat and temperature or tables.
- 4. Find mass terms, if necessary, using ideal gas law and/or open system relations for \dot{m} .